

## Synthesis of nano-Co<sub>3</sub>O<sub>4</sub>-based electrocatalysts and their performance in direct methanol fuel cells

X. Y Lu \*

*School of Materials Science and Engineering, East China University of Science and Technology, Shanghai, Fengxian District, 201424, China*

This study reports the synthesis of nano-Co<sub>3</sub>O<sub>4</sub> catalysts with tailored size and morphology using PEG as a dispersant, optimizing their application in DMFCs. By varying the molecular weight of PEG (400, 800, and 20000), the Co<sub>3</sub>O<sub>4</sub> catalysts exhibited distinct structural and catalytic properties. The Co<sub>3</sub>O<sub>4</sub> synthesized with PEG20000 showed the smallest crystallite size of 19.8 nm, the highest BET surface area of 168.7 m<sup>2</sup>/g, and a uniform morphology with well-dispersed nanoscale particles. Electrochemical analysis revealed that the Co<sub>3</sub>O<sub>4</sub>-modified Pt/C catalyst prepared with PEG20000 achieved a peak current density of 1.58 mA/cm<sup>2</sup>. The catalyst also demonstrated an onset potential of 0.19 V and a stability retention of 78.6% after 400 s of operation, outperforming Pt/C (68.4%). These enhancements are attributed to the synergistic effect providing oxygen species for intermediate oxidation and mitigating CO poisoning. The findings highlight the potential of Co<sub>3</sub>O<sub>4</sub>-modified Pt/C catalysts as efficient, cost-effective alternatives for DMFCs, with superior catalytic activity, stability, and methanol tolerance. This work offers insight into the role of dispersants in tailoring catalyst properties for energy applications.

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### 1. Introduction

The increasing demand for sustainable and efficient energy conversion technologies has placed significant emphasis on the development of advanced catalysts for electrochemical reactions. Among these, direct methanol fuel cells (DMFCs) have garnered considerable attention due to their potential as clean energy sources [1,2]. DMFCs operate by oxidizing methanol, producing electricity, water, and carbon dioxide [3]. However, the efficiency and durability of DMFCs are often hindered by the limitations of the catalysts employed [4–6]. Developing cost-effective, high-performance catalysts with robust stability and catalytic activity is therefore critical to advancing DMFC technology [7].

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\* Corresponding author: 18861630886@163.com

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Transition metal oxides, particularly cobalt-based oxides such as  $\text{Co}_3\text{O}_4$ , have emerged as candidates for ORR catalysis in DMFCs.  $\text{Co}_3\text{O}_4$  has gained prominence due to its unique physicochemical properties [8,9]. These include high thermal and chemical stability, abundant availability, and relatively low cost compared to noble metal catalysts such as platinum [10]. Furthermore,  $\text{Co}_3\text{O}_4$  exhibits significant catalytic activity for ORR due to its ability to facilitate multi-electron transfer reactions, making it a viable alternative to platinum-based materials [11,12]. However, despite these advantages,  $\text{Co}_3\text{O}_4$  suffers from inherent drawbacks, including low electrical conductivity and limited ion transport capacity, which restrict its catalytic performance and impede its practical application in DMFCs [13,14].

Addressing these limitations necessitates innovative strategies to enhance the catalytic efficiency and durability of  $\text{Co}_3\text{O}_4$ . One effective approach involves optimizing the synthesis process to control the particle size, morphology, and surface characteristics of  $\text{Co}_3\text{O}_4$  [15,16]. Additionally, tailoring the morphology of  $\text{Co}_3\text{O}_4$  can improve its interaction with reactants and facilitate efficient charge and mass transfer [17–19]. For instance, nanostructures such as spheres, rods, and cubes have been shown to exhibit distinct catalytic properties, underscoring the importance of morphological control in catalyst design. The use of dispersants during synthesis plays a pivotal role in achieving precise control over the size and morphology of  $\text{Co}_3\text{O}_4$  particles [20]. Polyethylene glycol (PEG), a widely used dispersant, has been demonstrated to significantly influence the nucleation and growth of  $\text{Co}_3\text{O}_4$  crystals [21]. By varying the molecular weight and concentration of PEG, it is possible to modulate the particle size, shape, and degree of agglomeration of  $\text{Co}_3\text{O}_4$ . PEG not only prevents particle aggregation by steric stabilization but also interacts with precursor ions, thereby influencing the crystallization process [22]. The selection of an optimal PEG type and concentration is therefore crucial for synthesizing  $\text{Co}_3\text{O}_4$  with desirable structural and catalytic properties [23].

In addition to optimizing the synthesis of  $\text{Co}_3\text{O}_4$ , further improvements in catalytic performance can be achieved through compositional modifications and hybridization with conductive materials [19]. Carbon-based materials are particularly effective as supports for  $\text{Co}_3\text{O}_4$  catalysts. These materials provide a high surface area for catalyst dispersion, and improve the overall stability of the catalyst [24]. By integrating  $\text{Co}_3\text{O}_4$  with carbon supports, it is possible to overcome the conductivity limitations of pure  $\text{Co}_3\text{O}_4$  while maintaining its intrinsic catalytic activity [25]. Moreover, the synergistic interaction between  $\text{Co}_3\text{O}_4$  and the carbon support can create additional active sites, further enhancing the catalytic performance. Another promising strategy to enhance the catalytic activity of  $\text{Co}_3\text{O}_4$  involves its modification with noble metals such as platinum [26]. Platinum, known for its superior catalytic performance in methanol oxidation and ORR, can be combined with  $\text{Co}_3\text{O}_4$  to create hybrid catalysts with improved activity and durability. In such configurations,  $\text{Co}_3\text{O}_4$  serves as a cost-effective and stable substrate that supports platinum nanoparticles, reducing the overall platinum loading while maintaining high catalytic efficiency [27]. This approach not only addresses the cost constraints associated with platinum but also leverages the complementary properties of  $\text{Co}_3\text{O}_4$  and platinum to achieve enhanced methanol oxidation and ORR performance.

This study aims to explore the synthesis of nano- $\text{Co}_3\text{O}_4$  catalysts with controlled size and morphology using PEG as a dispersant and to evaluate their performance in DMFCs. By systematically varying the molecular weight and concentration of PEG, the influence of dispersant properties of  $\text{Co}_3\text{O}_4$  is investigated. Furthermore, the study examines the modification of  $\text{Co}_3\text{O}_4$  with carbon supports and platinum to enhance its methanol oxidation activity and ORR performance. The

objectives of this work are threefold: (1) to synthesize  $\text{Co}_3\text{O}_4$  with optimized particle size and morphology through the use of PEG, (2) to develop  $\text{Co}_3\text{O}_4$ -based hybrid catalysts with improved conductivity and stability by integrating carbon supports, and (3) to enhance the catalytic activity of  $\text{Co}_3\text{O}_4$  by incorporating platinum.

## 2. Materials and methods

The synthesis of  $\text{Co}_3\text{O}_4$  was carried out using a chemical precipitation method, employing  $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  as the cobalt precursor, ammonium bicarbonate as the precipitating agent, and polyethylene glycol (PEG) of varying molecular weights (PEG400, PEG800, PEG20000, 99.99%, Shanghai Macklin Biochemical Co., Ltd.) as dispersants.

In a typical synthesis, 3.641 g of  $\text{Co}(\text{NO}_3)_2 \cdot 6\text{H}_2\text{O}$  was dissolved in 25 mL of absolute ethanol to prepare the cobalt precursor solution. Simultaneously, 2.0745 g of  $\text{NH}_4\text{HCO}_3$  was dissolved in water to prepare the precipitant solution. Both solutions were stirred separately for 20 minutes to ensure complete dissolution. In a three-neck round-bottom flask, 75 mL of absolute ethanol was mixed with a designated amount of PEG (either PEG400, PEG800, or PEG20000) and stirred at 45 °C in an oil bath for 1 hour. The cobalt nitrate and ammonium bicarbonate solutions were then added dropwise to the flask using separate constant-pressure funnels, maintaining a flow rate of approximately 15 drops per minute. Magnetic stirring was continued throughout the addition process to ensure thorough mixing.

The reaction mixture was allowed to proceed under stirring for 2 hours, followed by the addition of 5 mL of 30% hydrogen peroxide as an oxidizing agent. The resulting suspension was subjected to hydrothermal aging at 180 °C for 1 hour. The dried precursor was calcined in a furnace. The calcination was carried out at 350 °C for 2 hours, followed by further heating at 500 °C for 3 hours.

## 3. Results and discussion

The structural and morphological characteristics of  $\text{Co}_3\text{O}_4$  synthesized with varying molecular weights of polyethylene glycol (PEG400, PEG800, and PEG20000) were analyzed to understand the influence of PEG on crystallinity, particle size, surface area, and morphology. These properties are critical for determining the catalytic performance of  $\text{Co}_3\text{O}_4$  in DMFCs.

The XRD patterns of  $\text{Co}_3\text{O}_4$  synthesized with PEG400, PEG800, and PEG20000 are shown in Figure 1. All samples exhibited PDF #74-2120 spinel structure [28]. The absence of impurity peaks indicates that the synthesized  $\text{Co}_3\text{O}_4$  samples were of high purity.

The average crystallite sizes for PEG400, PEG800, and PEG20000 were calculated to be 25.4 nm, 22.7 nm, and 19.8 nm, respectively. The results demonstrate that increasing the molecular weight of PEG led to a significant reduction in crystallite size. This can be attributed to the enhanced dispersing effect of higher molecular weight PEG, which inhibits particle agglomeration during synthesis [29]. The smaller crystallite size of  $\text{Co}_3\text{O}_4$  synthesized with PEG20000 is expected to provide a larger active surface area.

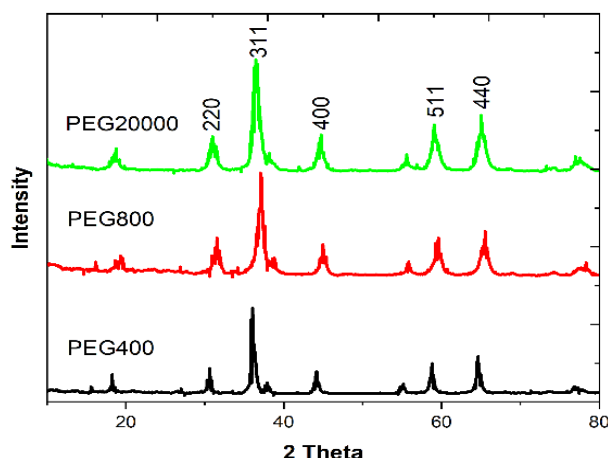


Fig. 1. XRD patterns of  $\text{Co}_3\text{O}_4$  synthesized with different PEG contents (PEG400, PEG800, PEG20000).

The  $\text{N}_2$  isotherms and corresponding pore size distributions of  $\text{Co}_3\text{O}_4$  samples synthesized with different PEG contents are presented in Figure 2. All samples exhibited type IV isotherms with H3 hysteresis loops [30]. The BET surface area of  $\text{Co}_3\text{O}_4$  increased significantly with the molecular weight of PEG, with values of  $87.5 \text{ m}^2/\text{g}$  for PEG400,  $112.3 \text{ m}^2/\text{g}$  for PEG800, and  $168.7 \text{ m}^2/\text{g}$  for PEG20000. Similarly, the pore volume increased from  $0.11 \text{ cm}^3/\text{g}$  for PEG400 to  $0.34 \text{ cm}^3/\text{g}$  for PEG20000. It revealed that all samples had average pore diameters in the range of 3.5–8.5 nm. The  $\text{Co}_3\text{O}_4$  synthesized with PEG20000 exhibited a narrower pore size distribution centered around 4.2 nm, while the samples synthesized with PEG400 and PEG800 had broader distributions. The higher surface area and optimized pore structure of the PEG20000 sample can facilitate efficient diffusion of reactants and products during the ORR and MOR, thereby enhancing catalytic performance.

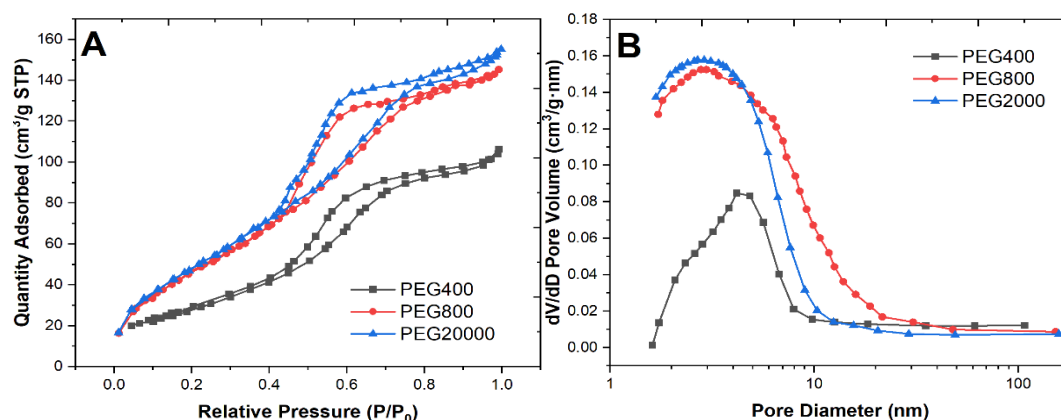
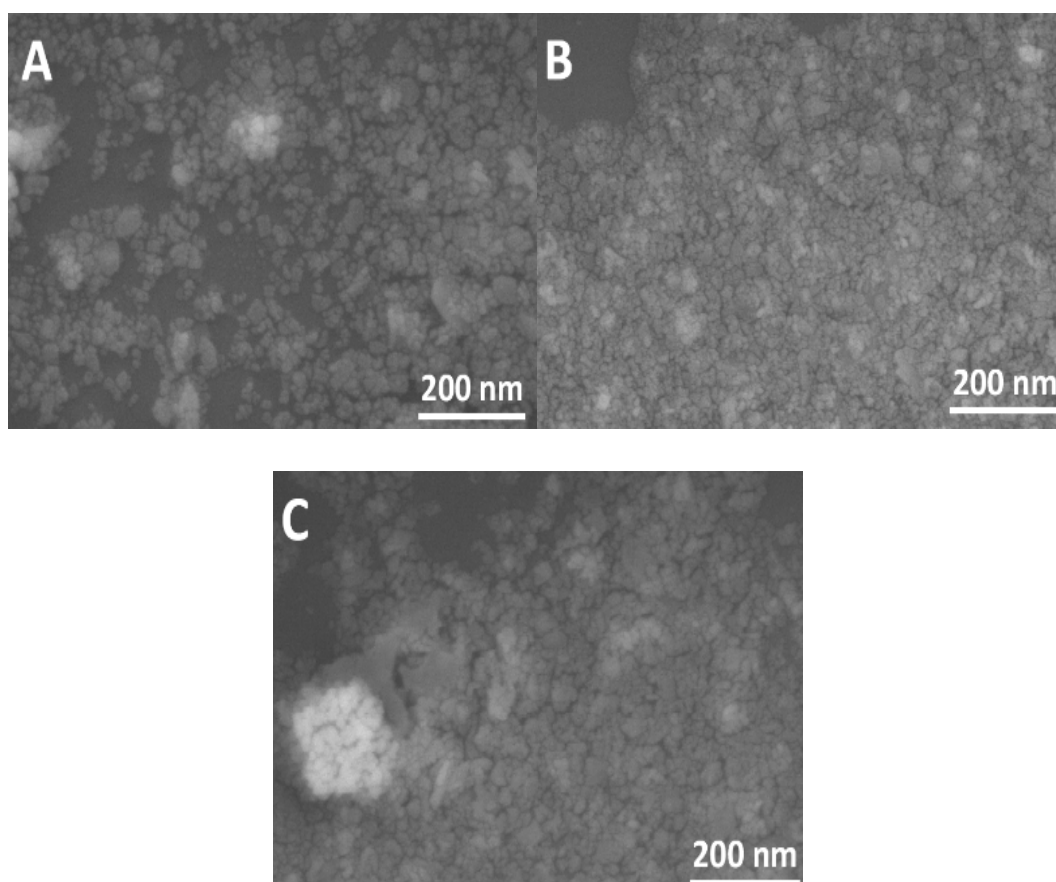


Fig. 2. (A)  $\text{N}_2$  isotherms and (B) pore size distributions of  $\text{Co}_3\text{O}_4$  synthesized with PEG400, PEG800, and PEG20000.

The SEM images of  $\text{Co}_3\text{O}_4$  prepared with PEG400, PEG800, and PEG20000 are shown in Figure 3. The sample synthesized with PEG400 exhibited irregularly shaped particles with significant agglomeration. The addition of PEG800 resulted in more uniform spherical particles with reduced agglomeration, indicating improved dispersion during synthesis. The most notable morphological improvement was observed in the sample synthesized with PEG20000, which exhibited well-dispersed nanoscale particles with a smooth surface and a uniform size distribution. The enhanced dispersion and reduced particle size in the presence of PEG20000 can be attributed to its higher molecular weight, which provides stronger steric hindrance and stabilizes the precursor solution during the synthesis process [31]. The uniform morphology and smaller particle size of the PEG20000 sample are expected to contribute to a higher density of active catalytic sites, which is critical for achieving enhanced electrochemical performance. The morphological differences observed in the SEM images align with the trends in crystallite size and surface area obtained from XRD and BET analyses. The  $\text{Co}_3\text{O}_4$  synthesized with PEG20000, having the smallest particle size, highest surface area, and most uniform morphology, is anticipated to exhibit superior catalytic activity in DMFC applications.



*Fig. 3. SEM images of  $\text{Co}_3\text{O}_4$  synthesized with (A) PEG400, (B) PEG800, and (C) PEG20000. The images reveal a transition from irregular agglomerates to well-dispersed nanoscale particles with increasing PEG molecular weight.*

The EDS spectrum, shown in Figure 4(A), confirmed the presence of cobalt (Co) and oxygen (O) as the primary elements, with no detectable impurities. The absence of peaks corresponding to other elements such as nitrogen or carbon indicates the complete removal of residual precursors and organic dispersants during the calcination process [32].

The elemental mapping images, presented in Figure 4(B), revealed a uniform distribution of Co and O. This homogeneity is critical for achieving consistent catalytic performance, as non-uniform elemental distribution can result in localized activity variations and reduced efficiency [33]. The uniformity observed in the mapping analysis suggests that the use of PEG20000 as a dispersant effectively prevented particle agglomeration and facilitated the even incorporation of oxygen into the  $\text{Co}_3\text{O}_4$  lattice. These findings align with the structural and morphological results, further supporting the suitability of PEG20000 for optimizing  $\text{Co}_3\text{O}_4$  synthesis.

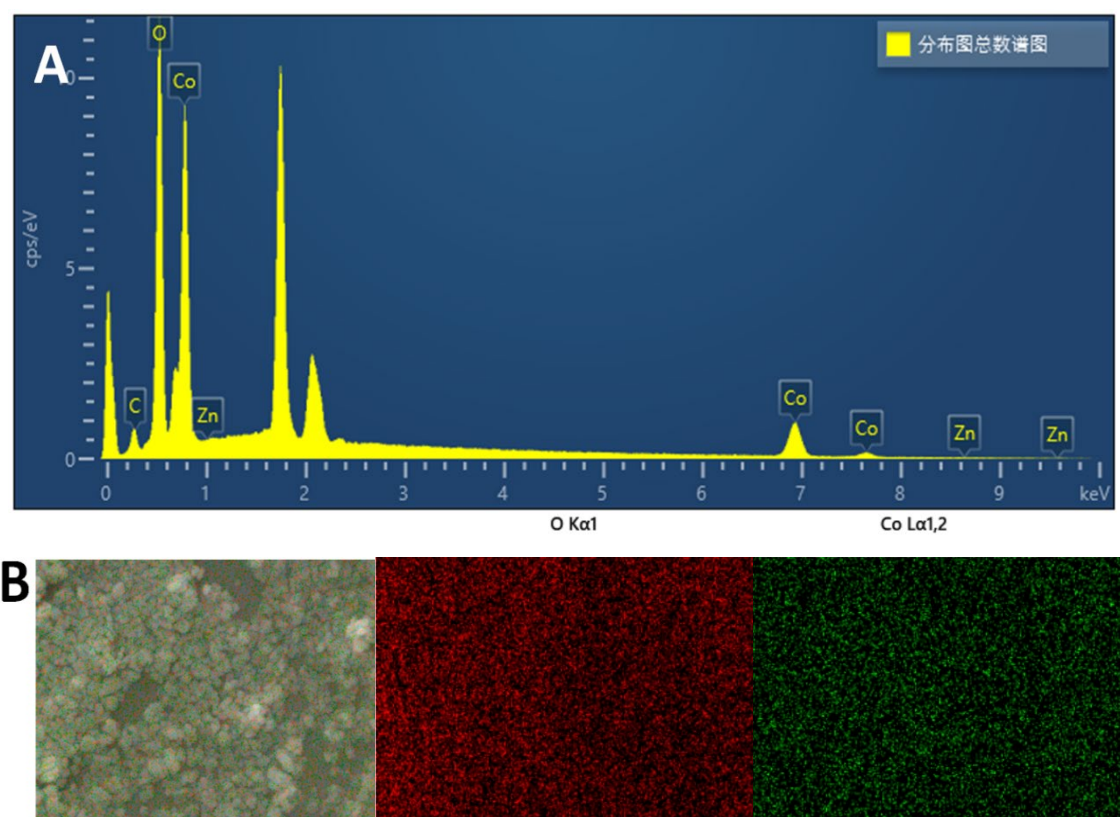
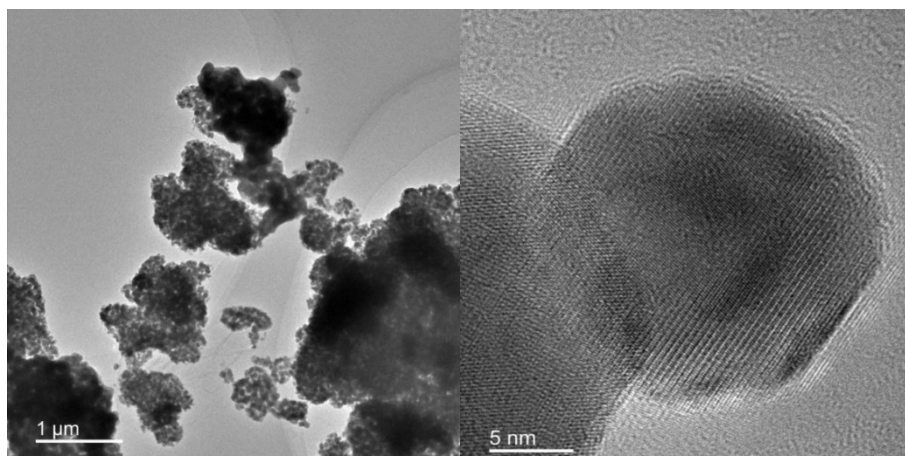


Fig. 4. (A) EDS spectrum and (B) elemental mapping of the optimized  $\text{Co}_3\text{O}_4$  synthesized with PEG20000, confirming the presence of Co and O without impurities.

The crystal structure and lattice characteristics of the optimized  $\text{Co}_3\text{O}_4$  sample were further investigated using HRTEM, as shown in Figure 5, revealed nanoscale particles with an average diameter of approximately 10 nm, consistent with the crystallite size estimated from XRD analysis. The particles exhibited a well-defined spinel structure, with clear lattice fringes corresponding to the (311) plane of  $\text{Co}_3\text{O}_4$ . This observation confirms the high crystallinity of the synthesized material.



*Fig. 5. TEM image of the optimized  $\text{Co}_3\text{O}_4$  synthesized with PEG20000, revealing nanoscale particles with clear lattice fringes corresponding to the (311) plane.*

The XPS spectra in Figure 6 show the Co 2p and O 1s spectra. The Co 2p spectrum, presented in Figure 6(A), exhibited two main peaks at binding energies of 780.2 eV and 795.3 eV [34]. These peaks were accompanied by satellite peaks at 785.1 eV and 802.4 eV [35]. The absence of significant contributions from  $\text{Co}^{2+}$  suggests that the sample predominantly consists of  $\text{Co}^{3+}$ , which is known to play a crucial role in enhancing catalytic activity for the MOR.

The O 1s spectrum, shown in Figure 6(B), displayed a strong peak at 529.6 eV, attributed to lattice oxygen ( $\text{O}^{2-}$ ) in the  $\text{Co}_3\text{O}_4$  spinel structure. A secondary peak at 531.2 eV was assigned to surface hydroxyl groups and adsorbed oxygen species, which are known to contribute to the catalytic activity by facilitating the adsorption and activation of methanol and oxygen molecules [36]. The relative intensity of the lattice oxygen peak compared to the surface oxygen peak indicates a high degree of crystallinity and minimal surface defects [37].

The chemical state analysis revealed that the optimized  $\text{Co}_3\text{O}_4$  sample synthesized with PEG20000 possesses a high concentration of  $\text{Co}^{3+}$  and lattice oxygen. The  $\text{Co}^{3+}$  sites enhance the adsorption and activation of methanol molecules, while the lattice oxygen enhances the oxidation of adsorbed intermediates, thereby improving the overall reaction kinetics [38]. The combination of high crystallinity, uniform elemental distribution, and favorable chemical states observed in the optimized  $\text{Co}_3\text{O}_4$  sample underscores its potential as an efficient electrocatalyst for DMFCs [39]. These properties are expected to translate into enhanced methanol oxidation activity, stability, and methanol tolerance compared to conventional catalysts.



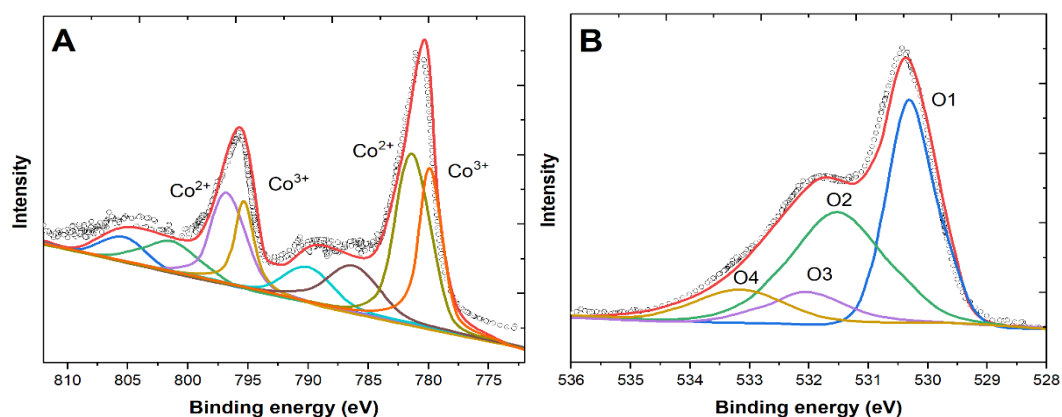


Fig. 6. (A) XPS spectrum of Co 2p for the optimized  $\text{Co}_3\text{O}_4$ , showing peaks characteristic of  $\text{Co}^{3+}$  in the spinel structure. (B) XPS spectrum of O 1s, highlighting contributions from lattice oxygen and surface hydroxyl groups.

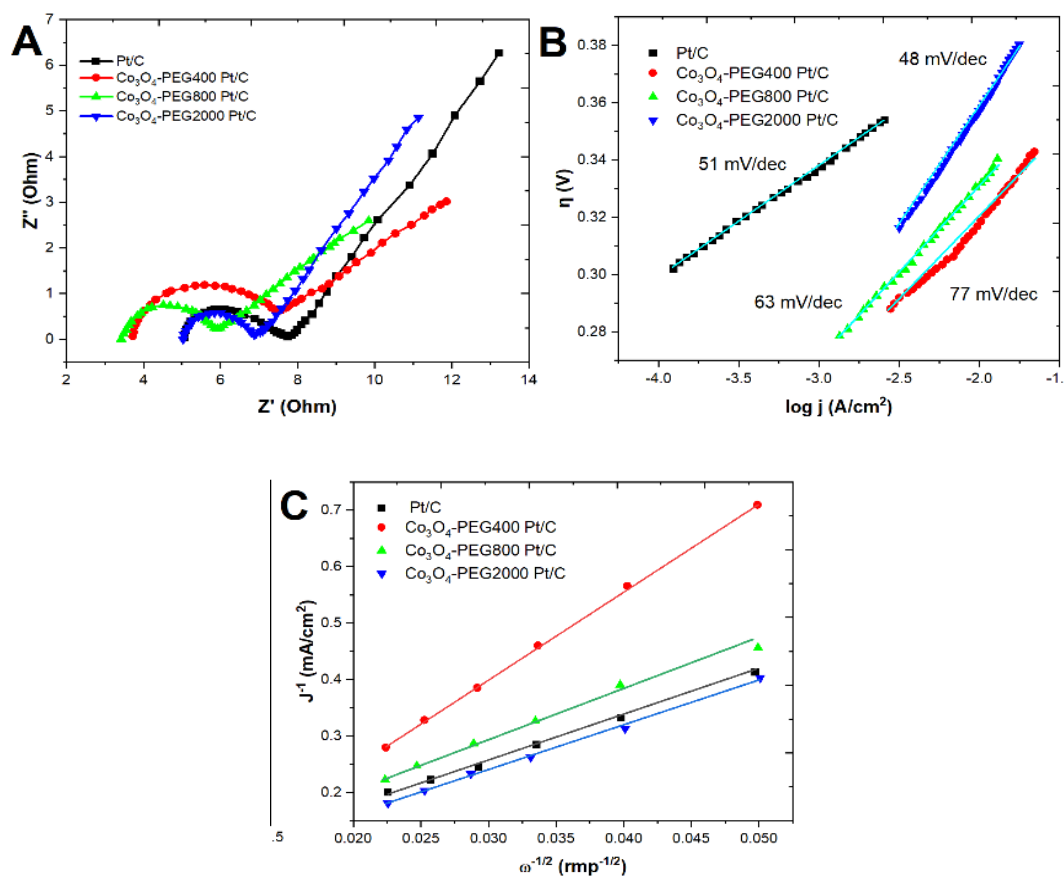


Fig. 7. (A) Nyquist impedance spectra for  $\text{Co}_3\text{O}_4$ -modified Pt/C catalysts synthesized with PEG400, PEG800, and PEG20000, together with commercial Pt/C. (B) Tafel plots (overpotential  $\eta$  versus  $\log j$ ) on  $\text{Co}_3\text{O}_4$ -modified Pt/C catalysts prepared with PEG400, PEG800, and PEG20000 and on commercial Pt/C. (C) Koutecky–Levich analysis of the optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C catalyst (PEG20000).



Nyquist plots (Figure 7A) display depressed semicircles whose diameters correspond to the  $R_{ct}$ . The PEG20000-derived catalyst exhibits the lowest  $R_{ct}$  (2.1  $\Omega$ ) relative to PEG800 (3.4  $\Omega$ ), PEG400 (4.7  $\Omega$ ) and commercial Pt/C (2.9  $\Omega$ ), indicating faster interfacial electron transport.

Figure 7(B) shows  $\eta$ -log  $j$  plots obtained from CV forward scans. Linear fits in the low-overpotential region yield Tafel slopes of 48 mV/dec (PEG20000), 63 mV/dec (PEG800), 77 mV/dec (PEG400) and 51 mV/dec (Pt/C). The smaller slope for the PEG20000 catalyst suggests a faster first electron-transfer step in the methanol dehydrogenation sequence.

Rotating-disk voltammograms (160–1600 rpm) were analysed using the K–L equation (Figure 7C). The linearity and slopes correspond to an electron-transfer number  $n = 3.9 \pm 0.1$ , confirming a near-complete four-electron ORR pathway.

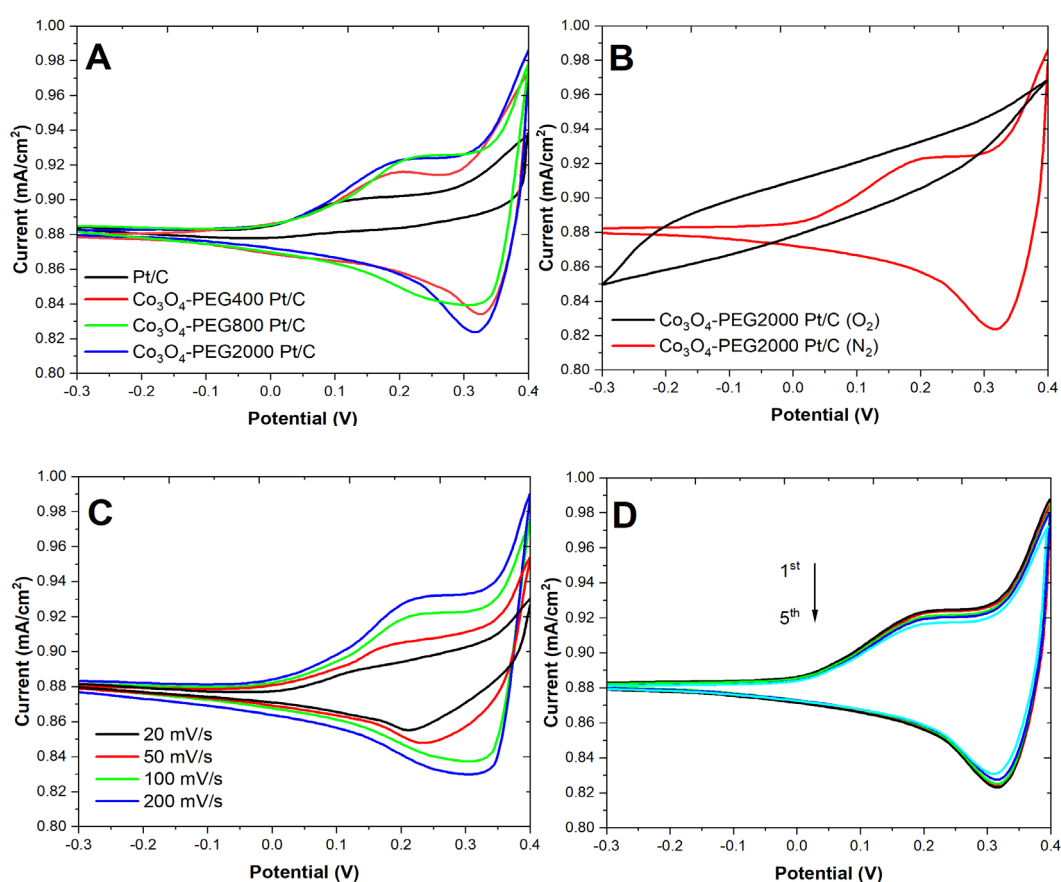


Fig. 8. (A) CV curves of  $\text{Co}_3\text{O}_4$ -modified Pt/C catalysts with varying PEG contents and commercial Pt/C. (B) CV curves of the optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C in  $\text{N}_2$  and  $\text{O}_2$ -saturated electrolytes. (C) CV curves of the optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C at different scan rates. (D) Stability test of the optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C over five cycles.

The electrocatalytic performance of  $\text{Co}_3\text{O}_4$ -modified Pt/C synthesized with varying PEG contents was evaluated using CV. The results are presented in Figure 8. Figure 8(A) illustrates the CV curves of  $\text{Co}_3\text{O}_4$ -modified Pt/C catalysts prepared with PEG400, PEG800, and PEG20000, alongside the commercial Pt/C catalyst. The optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C (with PEG20000)

exhibited a peak current density of 1.42 mA/cm<sup>2</sup> at 0.32 V, which was significantly higher than those prepared with PEG400 (0.87 mA/cm<sup>2</sup>) and PEG800 (1.12 mA/cm<sup>2</sup>). In comparison, the Pt/C catalyst showed a peak current density of 1.26 mA/cm<sup>2</sup> under the same conditions. The superior performance can be attributed to its higher surface area and smaller particle size, which provide more active sites for methanol oxidation [40].

The CV response of the optimized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C in N<sub>2</sub> and O<sub>2</sub>-saturated electrolytes is shown in Figure 8(B). In the N<sub>2</sub>-saturated electrolyte, no significant peaks were observed, indicating the absence of ORR activity [41]. Conversely, in the O<sub>2</sub>-saturated electrolyte, a pronounced reduction peak appeared at 0.28 V, confirming the ORR activity of the catalyst [42]. This demonstrates that the Co<sub>3</sub>O<sub>4</sub> component effectively enhances the oxygen adsorption and reduction capabilities of the catalyst, making it suitable for DMFC applications [43].

Figure 8(C) presents the CV curves of the optimized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C catalyst at scan rates ranging from 20 to 200 mV/s. As the scan rate increased, the peak current density increased linearly, indicating a diffusion-controlled process [44].

The stability of the optimized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C was evaluated over five consecutive CV cycles, as shown in Figure 8(D). The peak current density decreased by only 7.8% after five cycles, demonstrating excellent stability [45]. In comparison, the Pt/C catalyst exhibited a 15.4% reduction under the same conditions. The enhanced stability of the Co<sub>3</sub>O<sub>4</sub>-modified Pt/C can be attributed to the robust interaction between Co<sub>3</sub>O<sub>4</sub> and Pt, which mitigates Pt dissolution and aggregation during operation [46].

The long-term stability and methanol tolerance of the Co<sub>3</sub>O<sub>4</sub>-modified Pt/C were assessed using chronoamperometry (CA). Figure 9(A) shows the CA curves of Co<sub>3</sub>O<sub>4</sub>-modified Pt/C catalysts prepared with different PEG contents and the commercial Pt/C. The current density of the optimized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C (PEG20000) catalyst decreased from 0.98 mA/cm<sup>2</sup> to 0.74 mA/cm<sup>2</sup> after 400 seconds, corresponding to a retention rate of 75.5%. The retention rates for the PEG400- and PEG800-based catalysts were 62.3% and 68.7%, respectively, while the commercial Pt/C catalyst retained only 59.4% of its initial activity. The higher retention rate of the PEG20000-based catalyst demonstrates its superior methanol oxidation stability [47], which can be attributed to the uniform dispersion of Co<sub>3</sub>O<sub>4</sub> nanoparticles and their interaction with Pt.

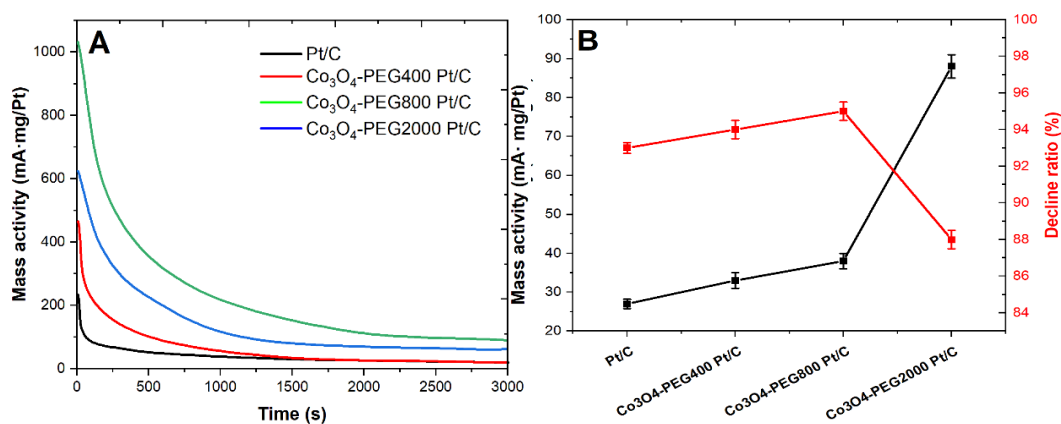


Fig. 9. (A) CA curves of Co<sub>3</sub>O<sub>4</sub>-modified Pt/C with varying PEG contents and Pt/C in methanol oxidation. (B) Retained activity and decay rates of the catalysts.

The retained activity and decay rates of the catalysts are summarized in Figure 9(B). The optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C catalyst exhibited the lowest decay rate of 0.60%/min, compared to 0.85%/min for the PEG400-based catalyst, 0.74%/min for the PEG800-based catalyst, and 1.02%/min for the Pt/C catalyst. This result highlights the effectiveness of the PEG20000-based synthesis in producing a catalyst with enhanced durability and methanol tolerance [48].

The catalytic performance and durability of  $\text{Co}_3\text{O}_4$ -modified Pt/C for the MOR were evaluated using CV and mass-specific activity analysis. The results, presented in Figure 10, highlight the influence of PEG content on the performance and demonstrate the advantages of the optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C catalyst.

Figure 10(A) shows the CV curves of  $\text{Co}_3\text{O}_4$ -modified Pt/C catalysts synthesized with PEG400, PEG800, and PEG20000. The optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C (PEG20000) exhibited a peak current density of 1.58  $\text{mA}/\text{cm}^2$  at 0.31 V, outperforming the catalysts prepared with PEG400 (1.02  $\text{mA}/\text{cm}^2$ ) and PEG800 (1.25  $\text{mA}/\text{cm}^2$ ). The Pt/C catalyst achieved a peak current density of 1.43  $\text{mA}/\text{cm}^2$  under identical conditions.

Additionally, the onset potential of the optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C catalyst was 0.19 V, which is comparable to that of the commercial Pt/C catalyst (0.18 V), indicating similar catalytic activation for MOR [49]. However, the  $\text{Co}_3\text{O}_4$ -modified Pt/C showed greater current stability during the forward and reverse scans, suggesting enhanced resistance to intermediate poisoning, such as CO, during methanol oxidation [50].

The mass-specific activity, calculated based on the peak current density and Pt loading, is illustrated in Figure 10(B). The optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C achieved a mass-specific activity of 0.92 A/mg Pt, significantly higher than those of the PEG400- and PEG800-based catalysts (0.59 A/mg Pt and 0.71 A/mg Pt, respectively) and the commercial Pt/C (0.84 A/mg Pt). This improvement highlights the synergistic effect, where  $\text{Co}_3\text{O}_4$  enhances the adsorption and activation of methanol while mitigating CO poisoning through its oxygen species [51].

The durability of the catalysts was further assessed by comparing the retained activity after 400 seconds of continuous operation. The optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C catalyst retained 78.6% of its initial activity, outperforming the PEG400- and PEG800-based catalysts (64.8% and 71.2%, respectively) and the commercial Pt/C catalyst (68.4%). This result underscores the role of the PEG20000 dispersant in producing a catalyst with enhanced durability and stability.

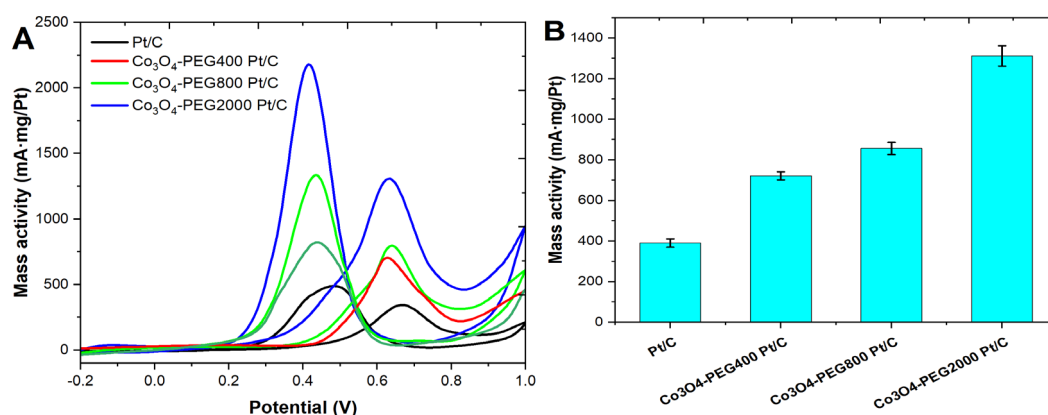


Fig. 10. (A) CV curves of  $\text{Co}_3\text{O}_4$ -modified Pt/C catalysts synthesized with varying PEG contents and Pt/C. (B) Mass-specific activity of  $\text{Co}_3\text{O}_4$ -modified Pt/C catalysts with varying PEG contents and commercial Pt/C.

Overall, the optimized  $\text{Co}_3\text{O}_4$ -modified Pt/C catalyst showed superior catalytic performance, methanol tolerance, and durability compared to both the other  $\text{Co}_3\text{O}_4$ -modified catalysts and the Pt/C. The findings confirm the potential of  $\text{Co}_3\text{O}_4$ -modified Pt/C as an effective and stable electrocatalyst for direct methanol fuel cells.

As depicted in Figure 11, small ( $\sim 3\text{--}5\text{ nm}$ ) Pt nanoparticles (dark grey) are uniformly dispersed on a high-surface-area carbon matrix (black), while  $10 \pm 2\text{ nm}$   $\text{Co}_3\text{O}_4$  nanocrystallites (blue) nucleate preferentially at the Pt|carbon interface. High-resolution TEM confirms coherent lattice contact between the Pt(111) and  $\text{Co}_3\text{O}_4$ (311) planes, creating abundant three-phase boundaries that shorten the diffusion path for reaction intermediates. The intimate juxtaposition of metallic (Pt) and redox-active oxide ( $\text{Co}_3\text{O}_4$ ) phases underpins the bifunctional mechanism discussed below.

Methanol molecules first adsorb on exposed Pt sites, forming surface-bound methoxy species ( $\text{CH}_3\text{O}^*$ ). Consecutive dehydrogenation steps yield  $\text{CO}^*$ —the strongly adsorbed intermediate that typically poisons pure-Pt catalysts. The low Tafel slope ( $48\text{ mV dec}^{-1}$ ) obtained for the PEG20000-derived catalyst (Figure 7B) indicates that this initial electron-transfer sequence is fast and that subsequent  $\text{CO}^*$  removal is rate-determining.  $\text{Co}_3\text{O}_4$  provides a reservoir of lattice oxygen ( $\text{O}^{2-}$ ) and surface  $\text{--OH}$  groups that can readily participate in oxidative chemistry. Under anodic bias,  $\text{Co}^{3+}$  centres at the oxide surface extract electrons to form highly reactive  $\text{O}^*$  species that spill-over to adjacent Pt sites. The  $\text{O}^*$  generated oxidises  $\text{CO}^*$  to  $\text{CO}_2$ , thereby freeing Pt active sites and mitigating poisoning. This bifunctional action rationalises the 22 % higher peak current density ( $1.58\text{ mA/cm}^2$ ) and the 10 % higher stability retention (78.6 %) compared with commercial Pt/C. Simultaneously, the  $\text{Co}^{3+} \rightleftharpoons \text{Co}^{2+}$  redox couple in  $\text{Co}_3\text{O}_4$  accelerates the four-electron oxygen-reduction pathway at the cathode, as evidenced by the  $n \approx 3.9$  value extracted from K–L plots. Because  $\text{CO}^*$  removal and  $\text{O}^*$  generation occur at the same interfacial region, the local concentration of reactive oxygen species is maximised, and the residence time of  $\text{CO}^*$  on Pt is minimised. Electrochemical impedance spectroscopy shows the lowest charge-transfer resistance ( $2.1\ \Omega$ ) for the PEG20000 catalyst, corroborating this synergistic hypothesis. The overall rate-determining step shifts from  $\text{CO}^*$  oxidation (pure Pt) to methanol dehydrogenation, thereby lowering the apparent Tafel slope and enhancing current output.

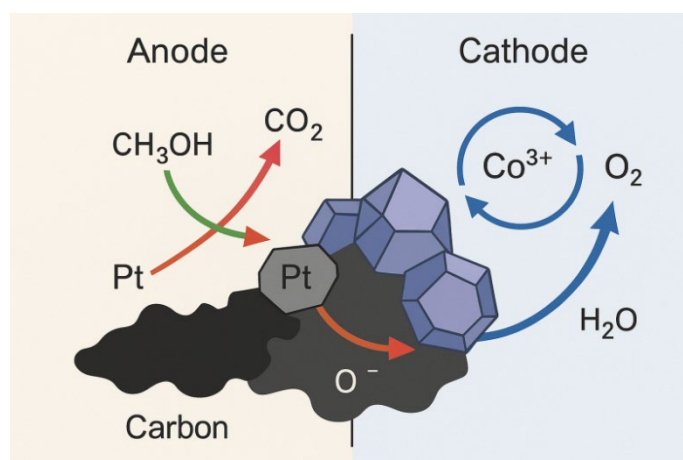


Fig. 11. Proposed bifunctional mechanism of methanol oxidation and oxygen reduction on the  $\text{Co}_3\text{O}_4$ -modified Pt/C.

To evaluate the performance of the synthesized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C catalysts in methanol oxidation, a comparison was made with other reported Co<sub>3</sub>O<sub>4</sub>-based catalysts from recent studies. Table 1 summarizes the MOR performance metrics, including peak current density, onset potential, mass-specific activity, and stability retention, for the optimized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C catalyst (synthesized with PEG20000) and other Co<sub>3</sub>O<sub>4</sub>-based catalysts.

The optimized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C catalyst in this study exhibited a peak current density of 1.58 mA/cm<sup>2</sup> and an onset potential of 0.19 V, which are comparable to or better than the values reported for Co<sub>3</sub>O<sub>4</sub>/N-doped carbon catalysts (1.45 mA/cm<sup>2</sup>, 0.21 V) and Co<sub>3</sub>O<sub>4</sub>-decorated graphene oxide catalysts (1.50 mA/cm<sup>2</sup>, 0.20 V). The mass-specific activity of 0.92 A/mg Pt achieved by the optimized catalyst exceeds the 0.85 A/mg Pt reported for Co<sub>3</sub>O<sub>4</sub>/graphene composites, indicating improved utilization of Pt and enhanced catalytic efficiency.

In terms of stability, the optimized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C retained 78.6% of its initial activity after 400 seconds of chronoamperometric testing, outperforming other catalysts such as Co<sub>3</sub>O<sub>4</sub>/graphene oxide (72%) and Co<sub>3</sub>O<sub>4</sub>-carbon nanotube hybrids (66%). This enhanced stability can be attributed to the uniform dispersion of Co<sub>3</sub>O<sub>4</sub> nanoparticles and their strong interaction with Pt, which mitigates Pt aggregation and dissolution during methanol oxidation.

The superior activity of the optimized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C catalyst is likely due to the synergistic effect of the Co<sub>3</sub>O<sub>4</sub> nanoparticles and the Pt/C support. The Co<sub>3</sub>O<sub>4</sub> nanoparticles provide oxygen species that facilitate the oxidation of intermediates such as CO, while the Pt/C support ensures efficient electron transfer and high catalytic activity. Furthermore, the use of PEG20000 as a dispersant during synthesis resulted in a catalyst with a high surface area, small particle size, and uniform morphology, all of which contribute to the enhanced catalytic performance. Overall, the results demonstrate that the optimized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C developed in this study outperforms many previously reported Co<sub>3</sub>O<sub>4</sub>-based catalysts.

*Table 1. Comparison of methanol oxidation performance metrics for the optimized Co<sub>3</sub>O<sub>4</sub>-modified Pt/C catalyst and other reported Co<sub>3</sub>O<sub>4</sub>-based catalysts.*

Catalyst	Peak Current Density (mA/cm <sup>2</sup> )	Onset Potential (V)	Mass-Specific Activity (A/mg Pt)	Stability Retention (%)	Ref.
Co <sub>3</sub> O <sub>4</sub> -modified Pt/C (PEG20000)	1.58	0.19	0.92	78.6	This work
Pt-Co <sub>3</sub> O <sub>4</sub> /NPC	1.42	0.20	0.81	81.4	[52]
Pt-Co <sub>3</sub> O <sub>4</sub> NP/NF	1.51	0.22	0.71	83.3	[53]
PtO <sub>x</sub> /CoO <sub>y</sub> @C-700	1.52	0.19	1.11	75.6	[54]
Pt-Co <sub>3</sub> O <sub>4</sub> -CDs/C	1.52	0.23	1.39	76.9	[28]

#### 4. Conclusion

The study successfully synthesized nano- $\text{Co}_3\text{O}_4$  catalysts with controlled size and morphology using PEG as a dispersant, demonstrating significant improvements in catalytic performance for DMFC applications.  $\text{Co}_3\text{O}_4$  synthesized with PEG20000 exhibited the smallest particle size (19.8 nm), highest surface area ( $168.7 \text{ m}^2/\text{g}$ ), and optimal pore structure, leading to superior catalytic activity. The  $\text{Co}_3\text{O}_4$ -modified Pt/C catalyst prepared with PEG20000 achieved a peak current density of  $1.58 \text{ mA}/\text{cm}^2$ , an onset potential of 0.19 V, and a mass-specific activity of  $0.92 \text{ A}/\text{mg Pt}$ , outperforming commercial Pt/C. Stability tests showed a retention rate of 78.6% after 400 s, significantly higher than the 68.4% retention of Pt/C. The enhanced performance was attributed to the synergistic effect of  $\text{Co}_3\text{O}_4$  and Pt, with  $\text{Co}_3\text{O}_4$  providing oxygen species to mitigate CO poisoning and improve methanol oxidation. These results highlight the potential of  $\text{Co}_3\text{O}_4$ -modified Pt/C catalysts as cost-effective and high-performance alternatives for DMFCs, with superior activity, stability, and methanol tolerance compared to existing catalysts.

#### References

- [1] M. A. Ud Din, M. Idrees, S. Jamil, S. Irfan, G. Nazir, M. A. Mudassir, M. S. Saleem, S. Batool, N. Cheng, R. Saidur, *Journal of Energy Chemistry* 77, 499 (2023); <https://doi.org/10.1016/j.jechem.2022.11.023>
- [2] C. Qin, S. Tian, W. Wang, Z.-J. Jiang, Z. Jiang, *Frontiers in Chemistry* 10, (2022); <https://doi.org/10.3389/fchem.2022.1073566>
- [3] Y.-Y. Feng, H.-S. Hu, R.-J. Liu, G. Deng, X.-Y. Wang, M. Zhu, *Chinese Journal of Structural Chemistry* 41, 2209080 (2022).
- [4] S. Li, Y. Zhang, Y. Han, F. Lv, B. Liu, L. Huo, *Applied Surface Science* 600, 154134 (2022); <https://doi.org/10.1016/j.apsusc.2022.154134>
- [5] D. Taxi, S. Shao, X. Maimaitiyiming, A. Sawut, M. Tursun, Z. Kuerban, H. Lin, *Separation and Purification Technology* 356, 129775 (2025); <https://doi.org/10.1016/j.seppur.2024.129775>
- [6] Y. Zuo, W. Sheng, W. Tao, Z. Li, *Journal of Materials Science & Technology* 114, 29 (2022); <https://doi.org/10.1016/j.jmst.2021.10.031>
- [7] Y. Fang, T. Zhang, Y. Zhang, J. Zhu, *Applied Catalysis A: General* 627, 118378 (2021); <https://doi.org/10.1016/j.apcata.2021.118378>
- [8] Y. Yu, S. You, J. Du, P. Zhang, Y. Dai, M. Liu, B. Jiang, N. Ren, J. Zou, *Chemical Engineering Journal* 403, 126441 (2021); <https://doi.org/10.1016/j.cej.2020.126441>
- [9] H. An, G.-H. An, H.-J. Ahn, *Journal of Alloys and Compounds* 645, 317 (2015); <https://doi.org/10.1016/j.jallcom.2015.05.105>
- [10] K.-H. Ye, S.-A. Zhou, X.-C. Zhu, C.-W. Xu, P. K. Shen, *Electrochimica Acta* 90, 108 (2013).
- [11] C. Xu, Z. Tian, P. Shen, S. P. Jiang, *Electrochimica Acta* 53, 2610 (2008).
- [12] M.-S. Ekrami-Kakhki, A. Naeimi, F. Donyagard, *International Journal of Hydrogen Energy* 44, 1671 (2019); <https://doi.org/10.1016/j.ijhydene.2018.11.102>



- [13] Y. Wu, J. Wang, G. Huang, S. Du, J. Lin, B. Zhou, Y. Lu, D. Wang, M. Li, L. Tao, S. Wang, *Journal of Power Sources* 541, 231643 (2022); <https://doi.org/10.1016/j.jpowsour.2022.231643>
- [14] Z. Li, S. Xu, Y. Shi, X. Zou, H. Wu, S. Lin, *Chemical Engineering Journal* 414, 128814 (2021); <https://doi.org/10.1016/j.cej.2021.128814>
- [15] D. K. Hassan, S. A. El-safty, K. A. Khalil, M. Dewidar, G. Abu el-maged, *International Journal of Electrochemical Science* 11, 8374 (2016); <https://doi.org/10.20964/2016.10.09>
- [16] N. Mamdouh, A. A. Farghali, W. M. A. El Rouby, A. Abdelwahab, *International Journal of Hydrogen Energy* 93, 878 (2024); <https://doi.org/10.1016/j.ijhydene.2024.10.398>
- [17] M. A. Shenashen, D. Hassen, S. A. El-Safty, H. Isago, A. Elmarakbi, H. Yamaguchi, *Chemical Engineering Journal* 313, 83 (2017); <https://doi.org/10.1016/j.cej.2016.12.003>
- [18] Y. Zhang, Y. Wang, J. Jia, J. Wang, *International Journal of Hydrogen Energy* 37, 17947 (2012); <https://doi.org/10.1016/j.ijhydene.2012.09.076>
- [19] G. Rajeshkhanna, G. Ranga Rao, *International Journal of Hydrogen Energy* 43, 4706 (2018); <https://doi.org/10.1016/j.ijhydene.2017.10.110>
- [20] Y. Ren, S. Zhang, H. Fang, X. Wei, P. Yang, *Journal of Energy Chemistry* 23, 801 (2014); [https://doi.org/10.1016/S2095-4956\(14\)60215-1](https://doi.org/10.1016/S2095-4956(14)60215-1)
- [21] D. Jin, Z. Li, L. Tang, Z. Wang, *Journal of Alloys and Compounds* 1008, 176651 (2024); <https://doi.org/10.1016/j.jallcom.2024.176651>
- [22] K. Pourzare, Y. Mansourpanah, S. Farhadi, M. M. Hasani Sadrabadi, I. Frost, M. Ulbricht, *Solid State Ionics* 351, 115343 (2020); <https://doi.org/10.1016/j.ssi.2020.115343>
- [23] R. Sundaresan, V. Mariyappan, T.-W. Chen, S.-M. Chen, M. Akilarasan, X. Liu, J. Yu, *Journal of Nanostructure in Chemistry* 14, 355 (2024); <https://doi.org/10.1007/s40097-023-00524-6>
- [24] M. Mehmood Shahid, A. Pandikumar, A. Moradi Golsheikh, N. Ming Huang, H. Ngee Lim, *RSC Advances* 4, 62793 (2014); <https://doi.org/10.1039/C4RA08952A>
- [25] C. Huang, Y. Zhang, X. Li, H. Cao, Y. Guo, C. Zhang, *Applied Catalysis B: Environmental* 319, 121909 (2022); <https://doi.org/10.1016/j.apcatb.2022.121909>
- [26] L. Qian, S. Luo, L. Wu, X. Hu, W. Chen, X. Wang, *Applied Surface Science* 503, 144306 (2020); <https://doi.org/10.1016/j.apsusc.2019.144306>
- [27] L. Qian, L. Gu, L. Yang, H. Yuan, D. Xiao, *Nanoscale* 5, 7388 (2013); <https://doi.org/10.1039/c3nr01104f>
- [28] Y. Sun, Y. Zhou, C. Zhu, L. Hu, M. Han, A. Wang, H. Huang, Y. Liu, Z. Kang, *Nanoscale* 9, 5467 (2017); <https://doi.org/10.1039/C7NR01727H>
- [29] G. V. Prasad, Y. C. Sekhar, K. Imran, V. Vinothkumar, T. H. Kim, *Journal of Physics and Chemistry of Solids* 196, 112304 (2025); <https://doi.org/10.1016/j.jpcs.2024.112304>
- [30] J. Du, S. You, X. Li, Y. Zhang, Y. Yu, Q. Li, F. Wang, N. Ren, J. Zou, *Journal of Power Sources* 478, 228707 (2020); <https://doi.org/10.1016/j.jpowsour.2020.228707>
- [31] S. Zhao, H. Wang, X. Liu, X. Cao, H. Yang, X. Kong, Q. Bu, Q. Liu, *Colloids and Surfaces A: Physicochemical and Engineering Aspects* 652, 129787 (2022);



<https://doi.org/10.1016/j.colsurfa.2022.129787>

- [32] K. Serbara Bejigo, K. Bhunia, J. Kim, C. Lee, S. Back, S.-J. Kim, *Journal of Energy Chemistry* 82, 148 (2023); <https://doi.org/10.1016/j.jechem.2023.03.042>
- [33] S. Zhao, H. Yang, Y. Liu, Y. Xing, G. Cui, Q. Liu, *New Journal of Chemistry* 45, 11245 (2021); <https://doi.org/10.1039/D1NJ01953H>
- [34] H. Wang, S. Li, G. Sun, G. Lu, Q. Bu, X. Kong, Q. Liu, *Inorganic Chemistry Communications* 145, 109984 (2022); <https://doi.org/10.1016/j.inoche.2022.109984>
- [35] M. M. Rahman, J. Ahmed, A. M. Asiri, S. Y. M. Alfaifi, H. M. Marwani, *Gels* 7, 235 (2021); <https://doi.org/10.3390/gels7040235>
- [36] S. Zafeiratos, F. Paloukis, G. Papakonstantinou, D. Teschner, M. Hävecker, E. Vass, P. Schnörch, A. Knop-Gericke, R. Schlögl, B. Moreno, E. Chinarro, J. R. Jurado, S. G. Neophytides, *Catalysis Today* 157, 250 (2010); <https://doi.org/10.1016/j.cattod.2010.03.030>
- [37] P. Arunachalam, M. A. Ghanem, A. M. Al-Mayouf, M. Al-shalwi, *Materials Letters* 196, 365 (2017); <https://doi.org/10.1016/j.matlet.2017.03.080>
- [38] H. S. Jadhav, A. Roy, W.-J. Chung, J. G. Seo, *New Journal of Chemistry* 41, 15058 (2017); <https://doi.org/10.1039/C7NJ03180G>
- [39] J. Acharya, B. Pant, G. P. Ojha, H.-S. Kong, M. Park, *Journal of Colloid and Interface Science* 602, 573 (2021); <https://doi.org/10.1016/j.jcis.2021.06.030>
- [40] Z. Wang, S. Zhou, W. Liao, Q. Wang, *International Journal of Hydrogen Energy* 47, 16056 (2022); <https://doi.org/10.1016/j.ijhydene.2022.03.093>
- [41] C. Lamiel, Y. R. Lee, M. H. Cho, D. Tuma, J.-J. Shim, *Journal of Colloid and Interface Science* 507, 300 (2017); <https://doi.org/10.1016/j.jcis.2017.08.003>
- [42] T. R. N. Kumar, M. Swamynadhan, S. Ghosh, B. Neppolian, *Sustainable Energy & Fuels* 6, 3573 (2022); <https://doi.org/10.1039/D2SE00660J>
- [43] K. Pourzare, Y. Mansourpanah, S. Farhadi, M. M. H. Sadrabadi, M. Ulbricht, *Energy* 239, 121940 (2022); <https://doi.org/10.1016/j.energy.2021.121940>
- [44] K. Baruah, P. Deb, *Dalton Transactions* 51, 4324 (2022); <https://doi.org/10.1039/D1DT03671H>
- [45] D. Z. Khater, R. S. Amin, A. E. Fetohi, M. Mahmoud, K. M. El-Khatib, *Scientific Reports* 13, 20184 (2023); <https://doi.org/10.1038/s41598-023-47450-9>
- [46] L. Gu, L. Qian, Y. Lei, Y. Wang, J. Li, H. Yuan, D. Xiao, *Journal of Power Sources* 261, 317 (2014); <https://doi.org/10.1016/j.jpowsour.2014.03.098>
- [47] M. A. Alvi, M. S. Akhtar, *Journal of Alloys and Compounds* 684, 524 (2016); <https://doi.org/10.1016/j.jallcom.2016.05.101>
- [48] M. Zhai, F. Chen, N. Wu, R. Guo, X. Zhang, T. Hu, M. Ma, *Applied Surface Science* 545, 149016 (2021); <https://doi.org/10.1016/j.apsusc.2021.149016>
- [49] K. Bhunia, E. Vijayakumar, N. P. Maria Joseph Raj, K. Serbara Bejigo, D. Kesavan, S.-J. Kim, *Chemical Engineering Journal* 473, 145028 (2023); <https://doi.org/10.1016/j.cej.2023.145028>

- [50] P. Arunachalam, M. N. Shaddad, A. S. Alamoudi, M. A. Ghanem, A. M. Al-Mayouf, *Catalysts* 7, 119 (2017); <https://doi.org/10.3390/catal7040119>
- [51] D. Wang, Q. Du, M. Li, L. Qian, F. Wang, *New Journal of Chemistry* 48, 14834 (2024); <https://doi.org/10.1039/D4NJ02109F>
- [52] Y. Zhang, Y. Sun, Z. Cai, S. You, X. Li, Y. Zhang, Y. Yu, N. Ren, J. Zou, *Journal of Colloid and Interface Science* 593, 345 (2021); <https://doi.org/10.1016/j.jcis.2021.02.125>
- [53] Y. Cao, J. Ge, M. Jiang, F. Zhang, X. Lei, *ACS Applied Materials & Interfaces* 13, 29491 (2021); <https://doi.org/10.1021/acsami.1c04045>
- [54] C. Ding, F. Dong, Z. Tang, *Journal of Electroanalytical Chemistry* 895, 115487 (2021); <https://doi.org/10.1016/j.jelechem.2021.115487>